

# The MoMaS Reactive Transport Benchmark

## Presentation of the Models

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Modelling Reactive Transport in Porous Media

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# Plan

- 1 Introduction
- 2 Mathematical model
- 3 Geometry and chemical data
- 4 Conclusions

## Design decisions

- **Compare** numerical methods and codes for reactive transport
- Bias towards **nuclear waste** disposal
- **Fixed** physical / chemical model
- **Simple** chemical system, with high **numerical** complexity
- No thermodynamic **database**

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## Consequences

- **Synthetic** chemical system
- **Small** number of species / reactions
- **Unrealistic** stoichiometry, equilibrium constants
- **Several** levels of difficulty

## Space discretization

**Features** Stability, numerical diffusion, efficiency

**Methods** Finite element / volumes, Ellam, particles, ...

# Main questions

## Space discretization

**Features** Stability, numerical diffusion, efficiency

**Methods** Finite element / volumes, Ellam, particles, ...

## Time discretization

- Explicit /implicit
- Lower /higher order
- Adaptive time step (heuristic, residual based)

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## Coupling methods

**Operator splitting** To iterate or not to iterate, OS error control

**Global** DSA, DAE, Newton (non-linear system solution, linear algebra, ...)

CPU time, memory

## Saturated flow : Darcy's law

$$\begin{cases} \omega u = -K \nabla h \\ \nabla \cdot (\omega u) = 0 \end{cases}$$

$\omega$  porosity,  $u$  Darcy velocity

## Transport model

$$\omega \frac{\partial (T_{M_j} + T_{F_j})}{\partial t} + \nabla \cdot (\omega u T_{M_j}) - \nabla \cdot (D \nabla T_{M_j}) = -\omega \sum_k a c_{k,j} f_k(C_i, C c_k)$$

Dispersion tensor  $D = \alpha_T \omega |u| I + (\alpha_L - \alpha_T) \omega \frac{u \otimes u}{|u|}$

$T_{M_j}$  (resp.  $T_{F_j}$ ) total mobile (resp. immobile) for concentration component  $j$ , kinetic source term, rate  $f_k(C_i, C c_k)$

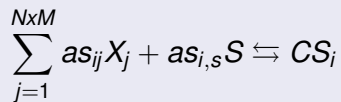
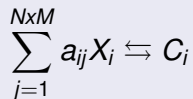


## Reactions

$$\sum_{j=1}^{N \times M} a_{ij} X_j \rightleftharpoons C_i$$

$$\sum_{j=1}^{N \times M} a_{sij} X_j + a_{s,i,s} S \rightleftharpoons C S_i$$

## Reactions



## Mass action laws

$$C_i = K_i \prod_{j=1}^{N \times M} X_j^{a_{ij}}$$

$$C S_i = K s_i \prod_{j=1}^{N \times M} X_j^{a s_{ij}} S^{a s_{i,s}}$$

## Reactions

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$$\sum_{j=1}^{N \times M} a_{sij} X_j + a_{s,i,s} S \rightleftharpoons CS_i$$

## Mass action laws

$$C_i = K_i \prod_{j=1}^{N \times M} X_j^{a_{ij}}$$

$$CS_i = K_{s,i} \prod_{j=1}^{N \times M} X_j^{a_{sij}} S^{a_{s,i,s}}$$

## Conservation of mass

$$T_j = X_j + \sum_{i=1}^{NcM} a_{ij} C_i + \sum_{i=1}^{NcS} a_{sij} CS_i$$

$$TS = S + \sum_{i=1}^{NcS} a_{s,i,s} CS_i$$

Formation of immobile species  $C_c$  :



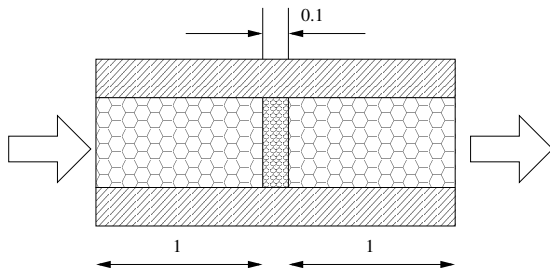
Rate law :

$$\frac{dC_c}{dt} = \left( 0.2 \frac{C_3^3}{X_4^2} - 1 \right) k, \quad \text{with } C_c \geq 0,$$

$$k = \begin{cases} 10^{-2} & \text{if } 0.2 \frac{C_3^3}{X_4^2} \geq 1 \\ 10 & \text{otherwise.} \end{cases}$$

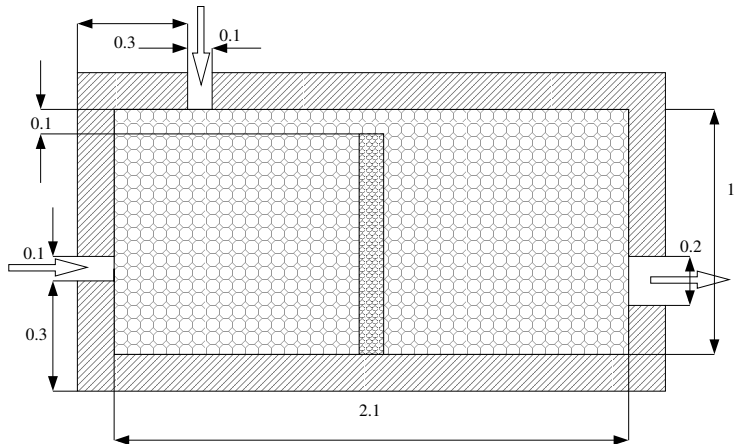
Initial condition :  $C_c(t = 0) = 5$ .

# Geometry : 1D model



	Medium A	Medium B
Porosity $\omega[-]$	0.25	0.5
Permeability $K (LT^{-1})$	$10^{-2}$	$10^{-5}$
Dispersivity $\alpha_L[L]$	$10^{-2}$ (10)	$6 \cdot 10^{-2}$ (60)
Dispersivity $\alpha_T[L]$	$10^{-3}$ (1)	$6 \cdot 10^{-3}$ (6)
Concentration $T_s$	1	10

# Geometry : 2D model



## Morel tableau

	$X_1$	$X_2$	$X_3$	$X_4$	$S$	$K$
$C_1$	0	-1	0	0	0	$10^{-12}$
$C_2$	0	1	1	0	0	1
$C_3$	0	-1	0	1	0	1
$C_4$	0	-4	1	3	0	0.1
$C_5$	0	4	3	1	0	$10^{35}$
$CS_1$	0	3	1	0	1	$10^6$
$CS_2$	0	-3	0	1	2	$10^{-1}$
<b>Total</b>	$T_1$	$T_2$	$T_3$	$T_4$	$TS$	
Init. medium A (B)	0	-2	0	2	1 (10)	
injection $t \in [0, 5000]$	0.3	0.3	0.3	0		
Leaching $t \geq 5000$	0	-2	0	2		

# Chemistry : medium test case

## Morel tableau

	$X_1$	$X_2$	$X_3$	$X_4$	$S$	$K$
$C_1$	0	-1	0	0	0	$10^{-12}$
$C_2$	0	1	1	0	0	1
$C_3$	0	-1	0	1	0	1
$C_4$	0	-4	1	3	0	0.1
$C_5$	0	4	3	1	0	$10^{35}$
$C_6$	0	10	3	0	0	$10^{32}$
$C_7$	0	-8	0	2	0	$10^{-4}$
$CS_1$	0	3	1	0	1	$10^6$
$CS_2$	0	-3	0	1	2	$10^{-1}$
<b>Total</b>	$T_1$	$T_2$	$T_3$	$T_4$	$TS$	
Init. medium A (B)	0	-3 (-9)	0	1 (3)	1 (10)	
injection $t \in [0, 5000]$	0.3	0.3	0.3	0		
Leaching $t \geq 5000$	0	-3	0	1.5		



# Chemistry : hard test case

## Morel tableau

	$X_1$	$X_2$	$X_3$	$X_4$	$X_5$	$S$	$K$
$C_1$	0	-1	0	0	0	0	$10^{-12}$
$C_2$	0	1	1	0	0	0	1
$C_3$	0	-1	0	1	0	0	1
$C_4$	0	-4	1	3	0	0	0.1
$C_5$	0	4	3	1	0	0	$10^{35}$
$C_6$	0	10	3	0	0	0	$10^{32}$
$C_7$	0	-8	0	2	0	0	$10^{-4}$
$CS_2$	0	-3	0	1	0	2	$10^{-1}$
$CP_1$	0	3	1	0	0	0	$10^{10}$
$CP_2$	0	1	0	0	1	0	20
<b>Total</b>	$T_1$	$T_2$	$T_3$	$T_4$	$T_5$	$TS$	
Init. A (B)	0	-30 (-90)	0	10 (30)	0	1 (10)	
inj.	0.3	0.3	0	0		0.3	
Leach.	0	-3	0	1.5	0		

# Conclusions

## Main difficulties

- **Very large** difference in the size of equilibrium constants
- **Large** stoichiometric coefficients, gives very **nonlinear** behavior
- **Long** simulation time
- Correct resolution of **transport** for 2D case

## Limitations

- Artificial chemistry, unrealistic ?
- Easy subset aimed at mathematicians
- Only one situation, limited conclusions